

***Retention control system for  
the wet-end section in a paper machine.***

**Yoshitatsu Mori, Pulp and Paper Research Laboratory.  
Oji Paper Co., Ltd.**

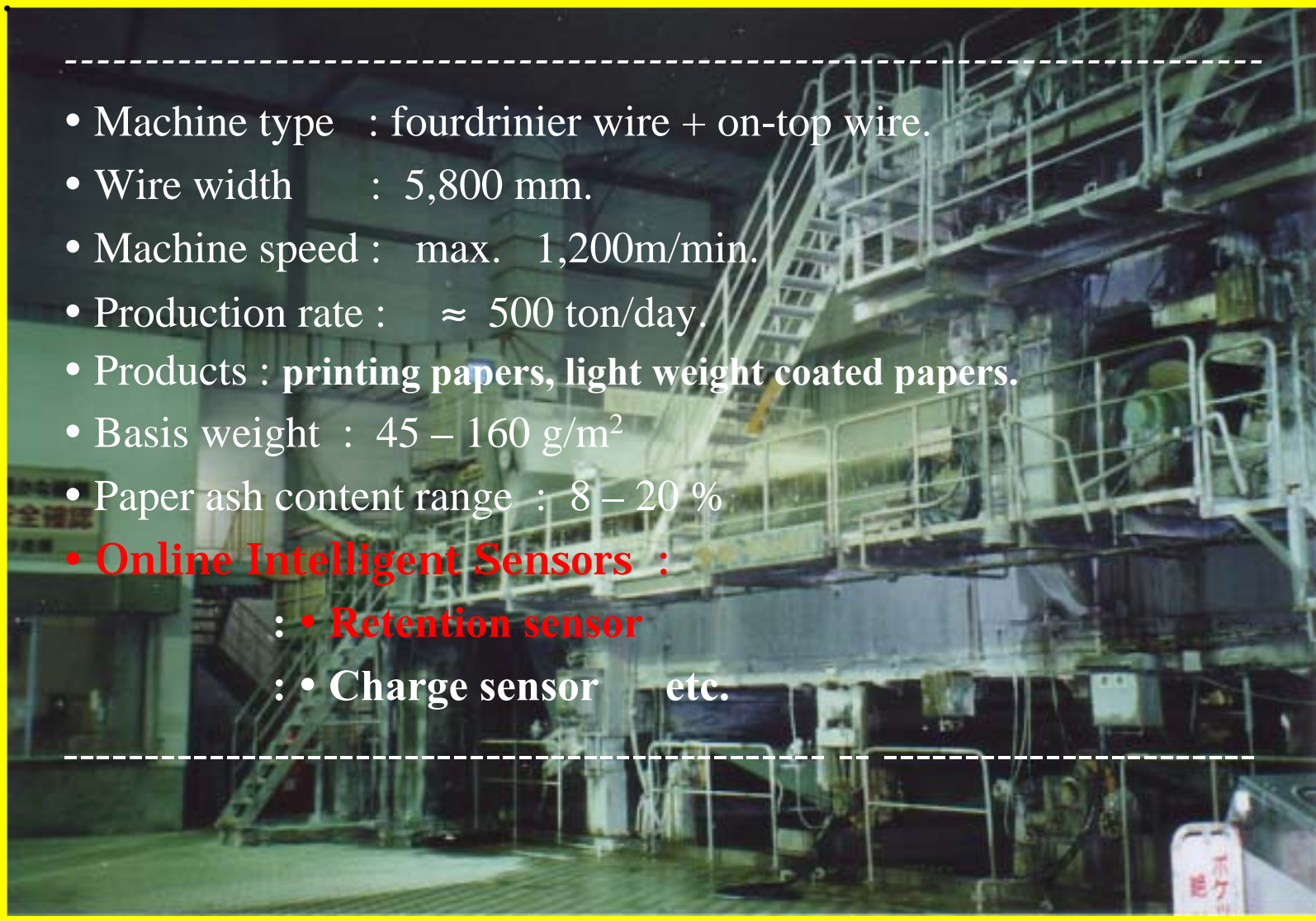
**Naoki Imai, Technology Div. Oji Paper Co., Ltd.**

**Yoshinobu Hara, Michiaki Nishimura, Shirou Hirano,  
Kure Mill. Oji Paper Co., Ltd.**

**( E-mail : [yoshitatsu-mori@ojipaper.co.jp](mailto:yoshitatsu-mori@ojipaper.co.jp) )**

## *Kure Mill : No.5 paper machine. (wire part)*

- Machine type : fourdrinier wire + on-top wire.
- Wire width : 5,800 mm.
- Machine speed : max. 1,200m/min.
- Production rate :  $\approx$  500 ton/day.
- Products : printing papers, light weight coated papers.
- Basis weight : 45 – 160 g/m<sup>2</sup>
- Paper ash content range : 8 – 20 %
- **Online Intelligent Sensors :**
  - Retention sensor
  - Charge sensor etc.

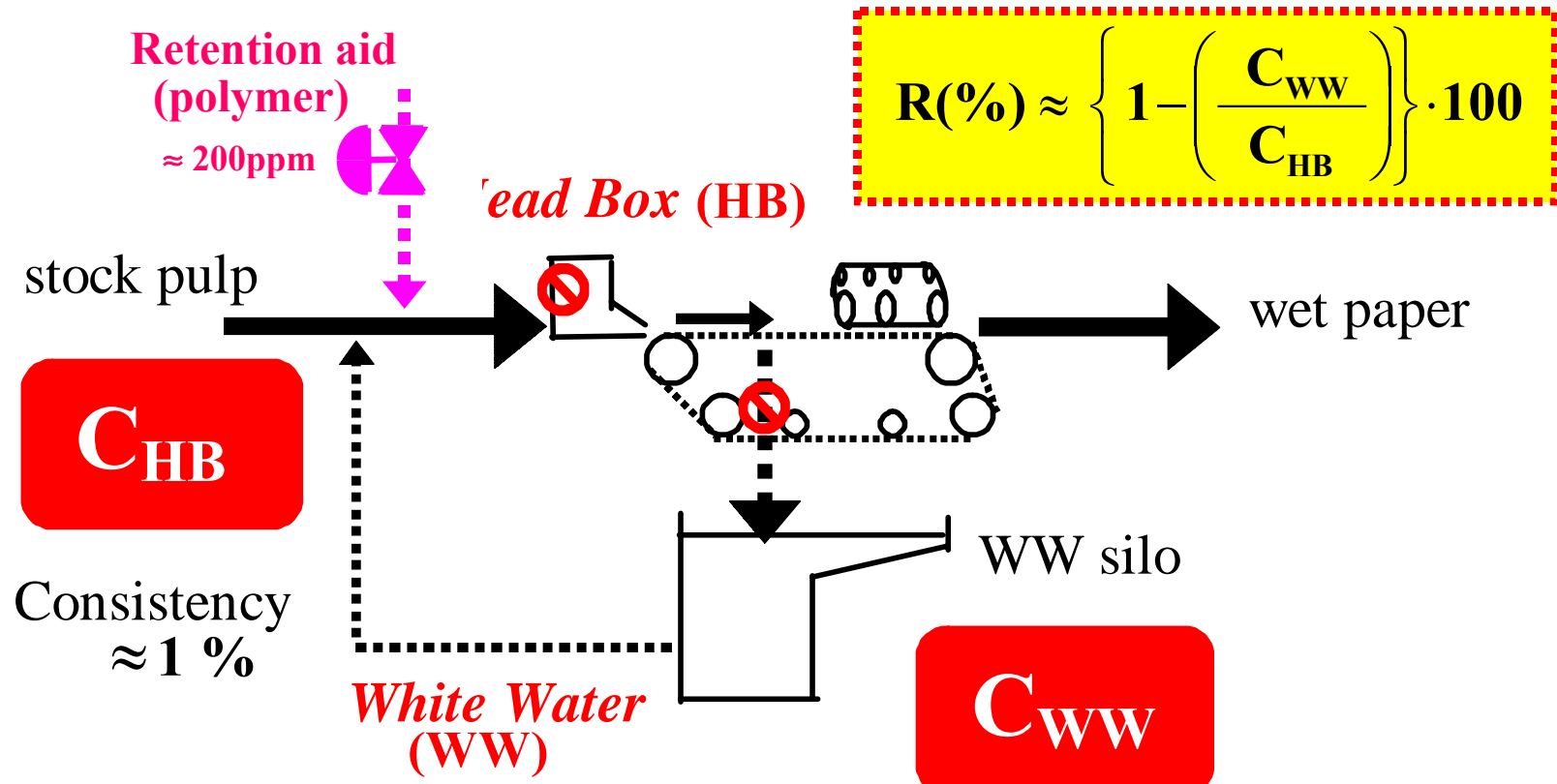


## The purpose of the “Retention Control”.

- Stabilize the filtration conditions of a paper machine.
  - filtrated white water consistency
  - total retention of the wire-part
- Stabilize the operation and the quality of the paper products.



# Paper Machine : Retention control



\* Retention values (on average)  
 $R_{pulp} \approx 70 \%$     $R_{ash} \approx 40 \%$   
 $R_{total} \approx 60 \%$

wire part



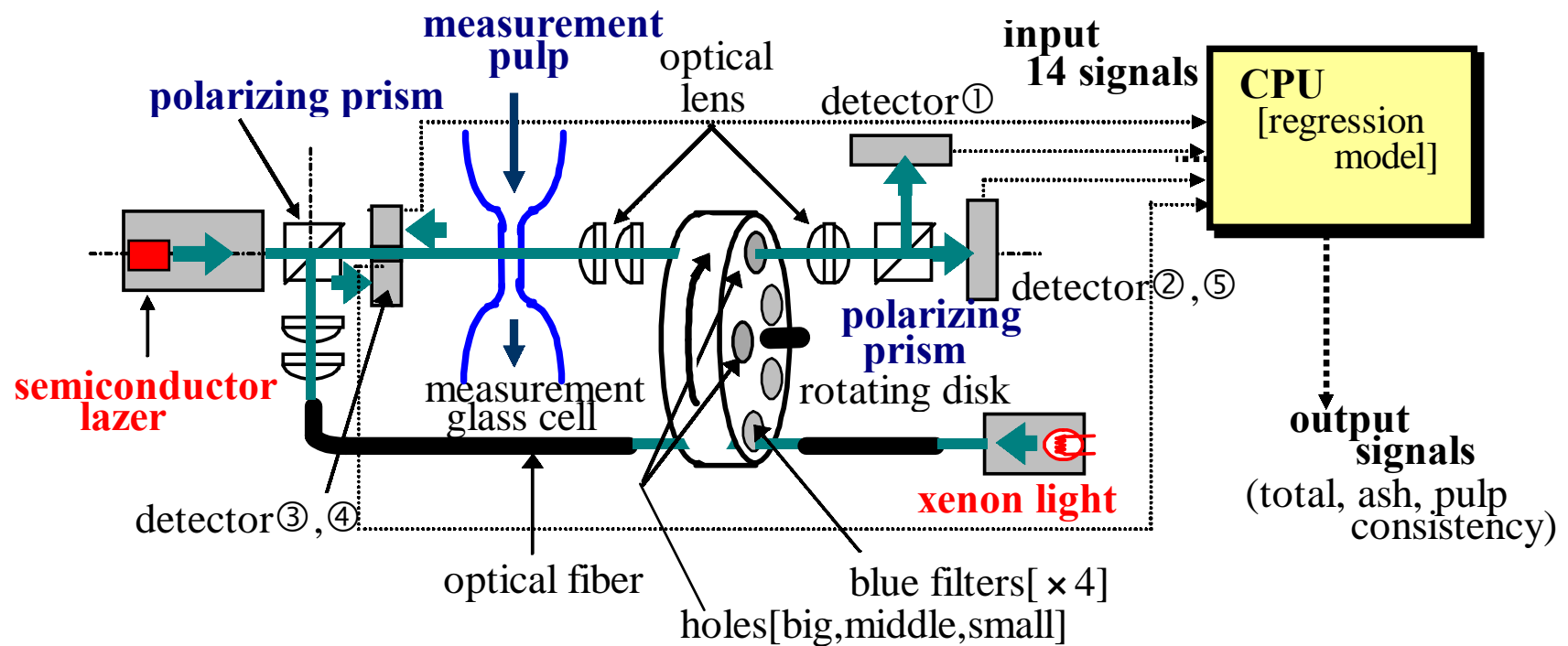
- Optical sensor.
- CPU unit.

- Total conc. 1.5%
- Ash conc. 0.8%

- 2 systems.  
(HB & WW)

\* not only to use for only the monitoring sensor but also use for available control system.

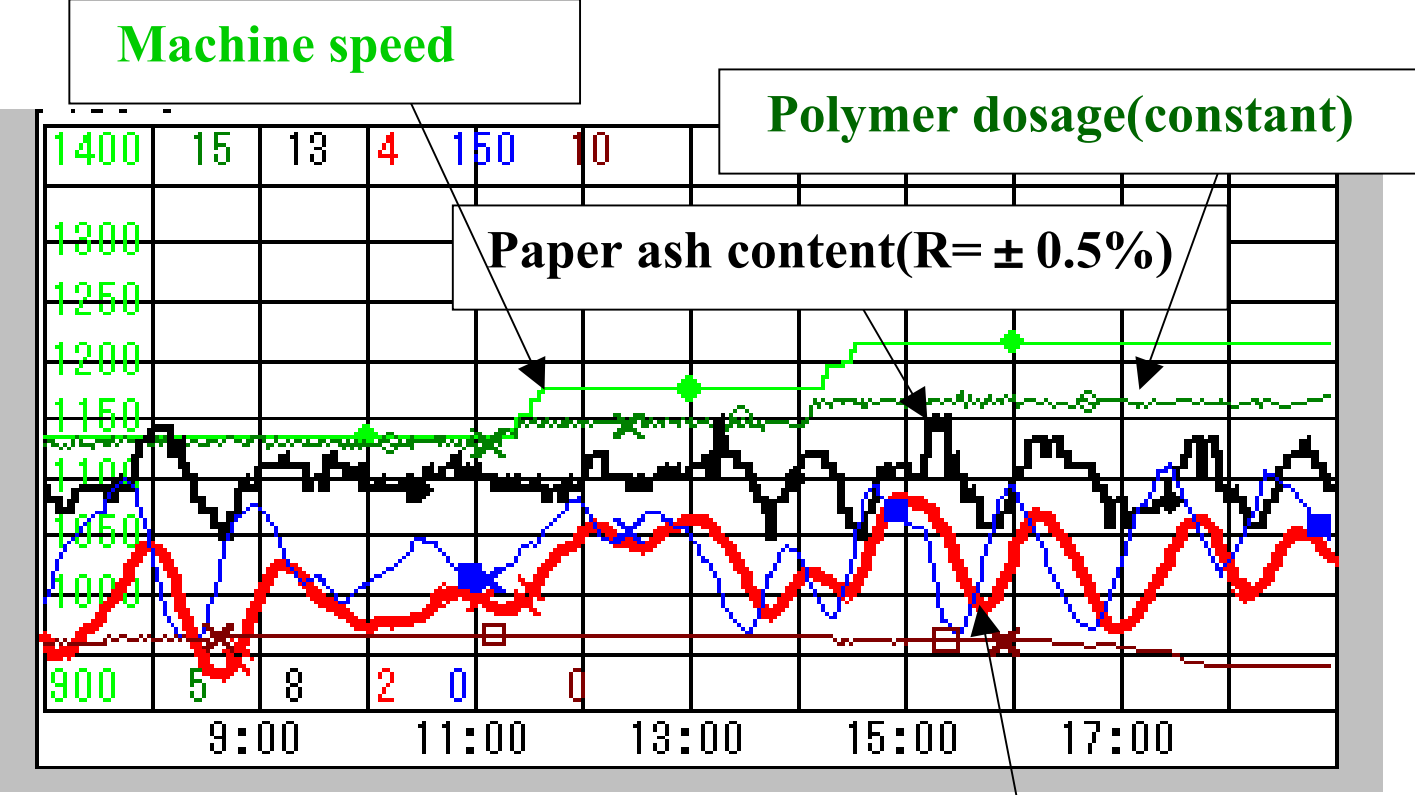
**Low consistency pulp and ash sensor  
( Metso Automation/Finland : RMi )**



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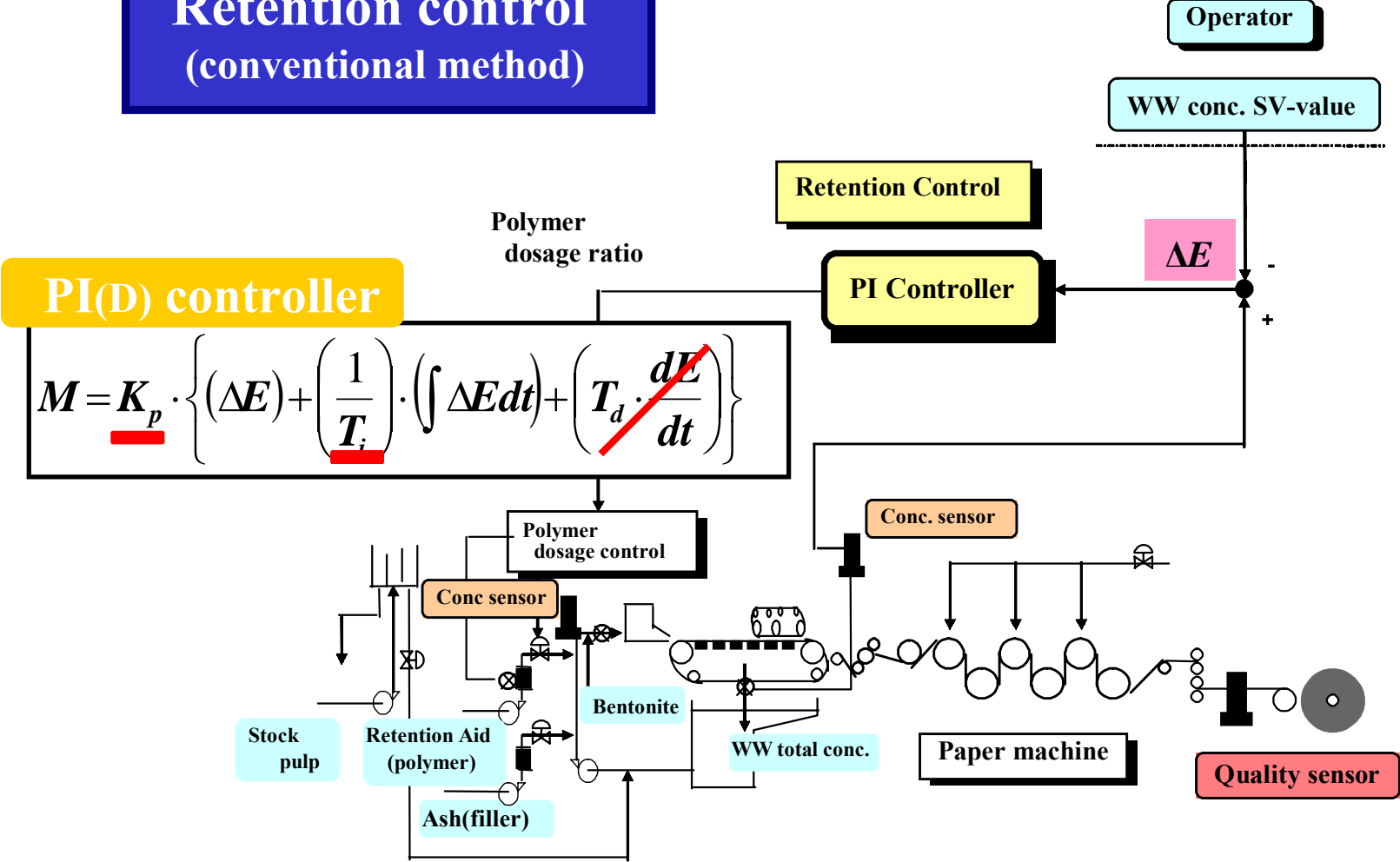
**DCS Operation Room (*Kure* Mill : No.5 paper machine)**



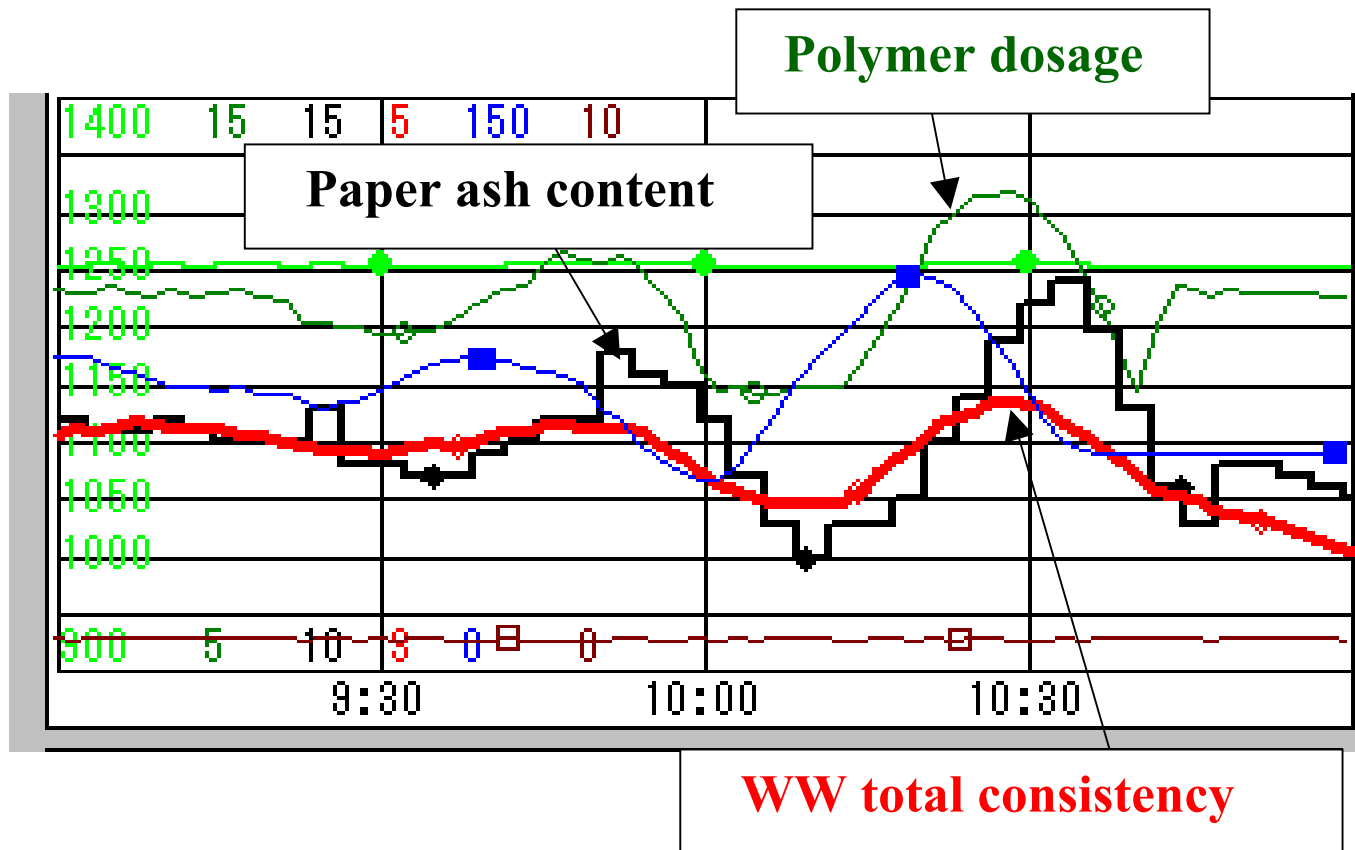
**No retention control**



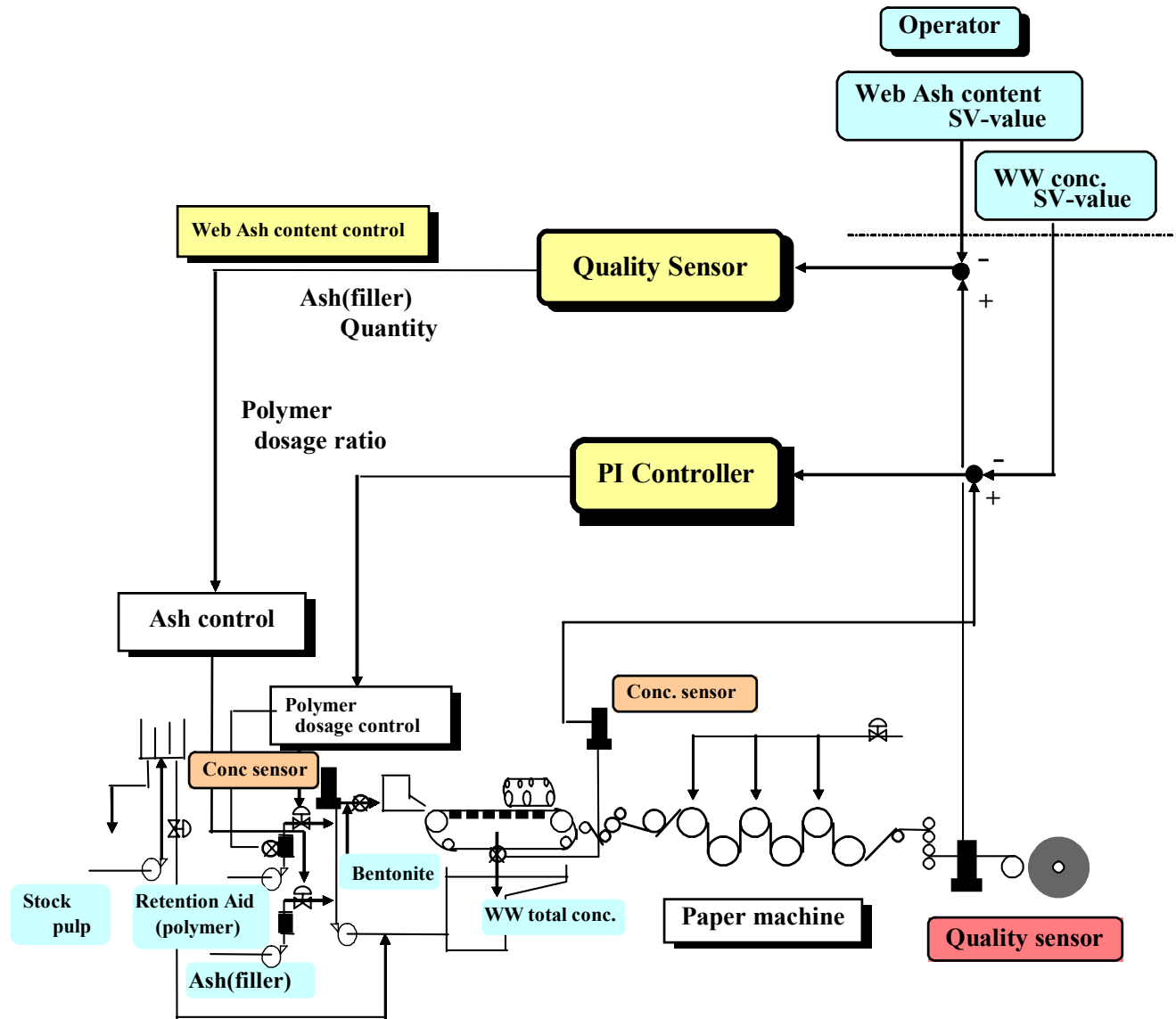
# Retention control (conventional method)



# PI-feedback control by retention aid

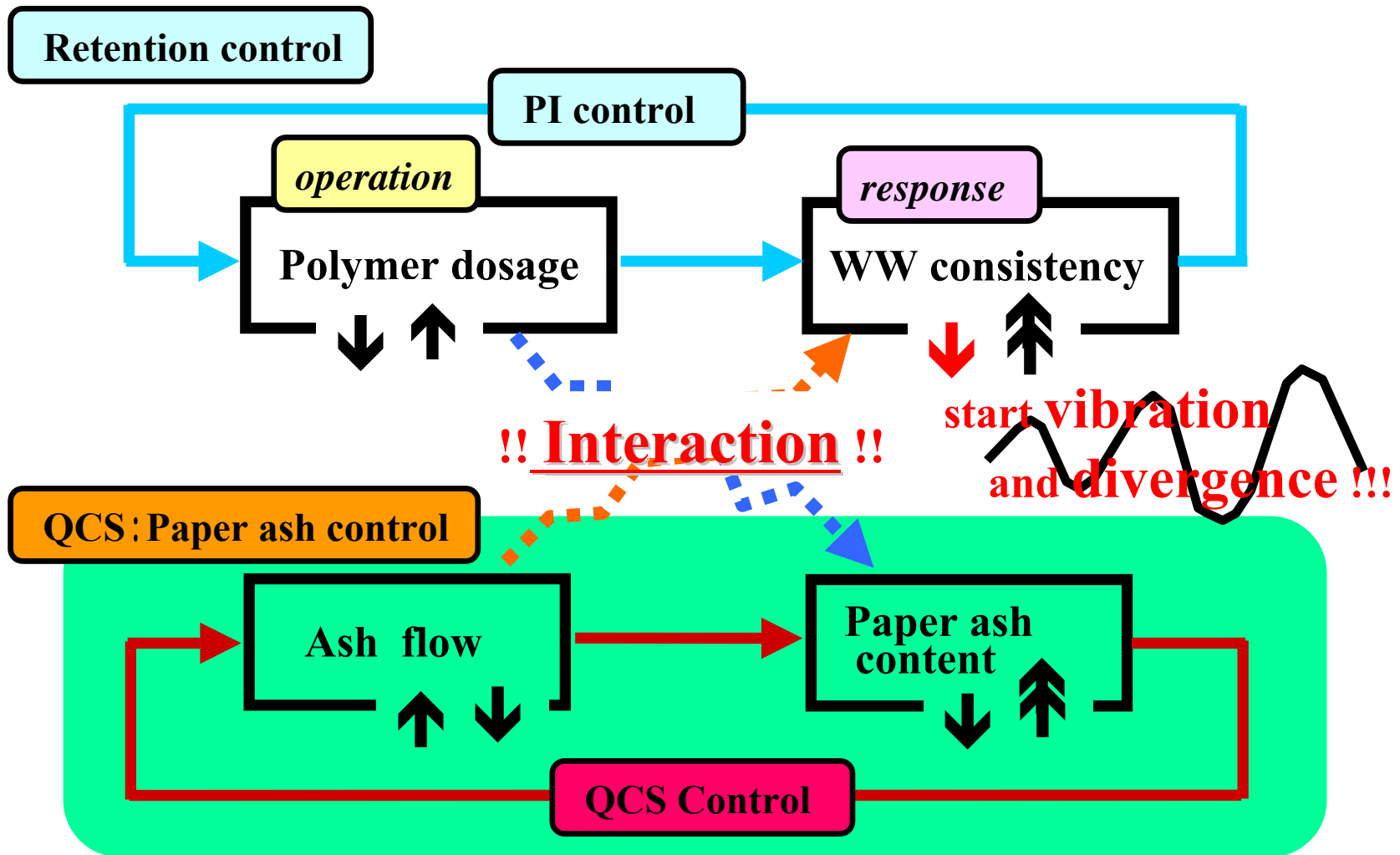


**Control result : PI-feedback control**



**Interaction with PI-feedback control**

*ex. Cause of the vibration by mutual interaction.*



## -- Problems --

- *strong Interaction*

*“Retention PI-control”* ( *WW consistency* ) of *DCS*

*and*

*“Paper Ash content control”*

*of QCS (Quality Control System)*

## -- Method of approach --

◆ *conventional “PI-control”*

*+ “Decoupling control”.*

## Transfer functions of the process

*control item*  
*operation*

Quality Sensor control  
Ash content

WW total  
consistency

Ash flow

$$G_{11} = \frac{+ K_{11} \cdot e^{-126 \cdot S}}{1 + 75 \cdot S}$$

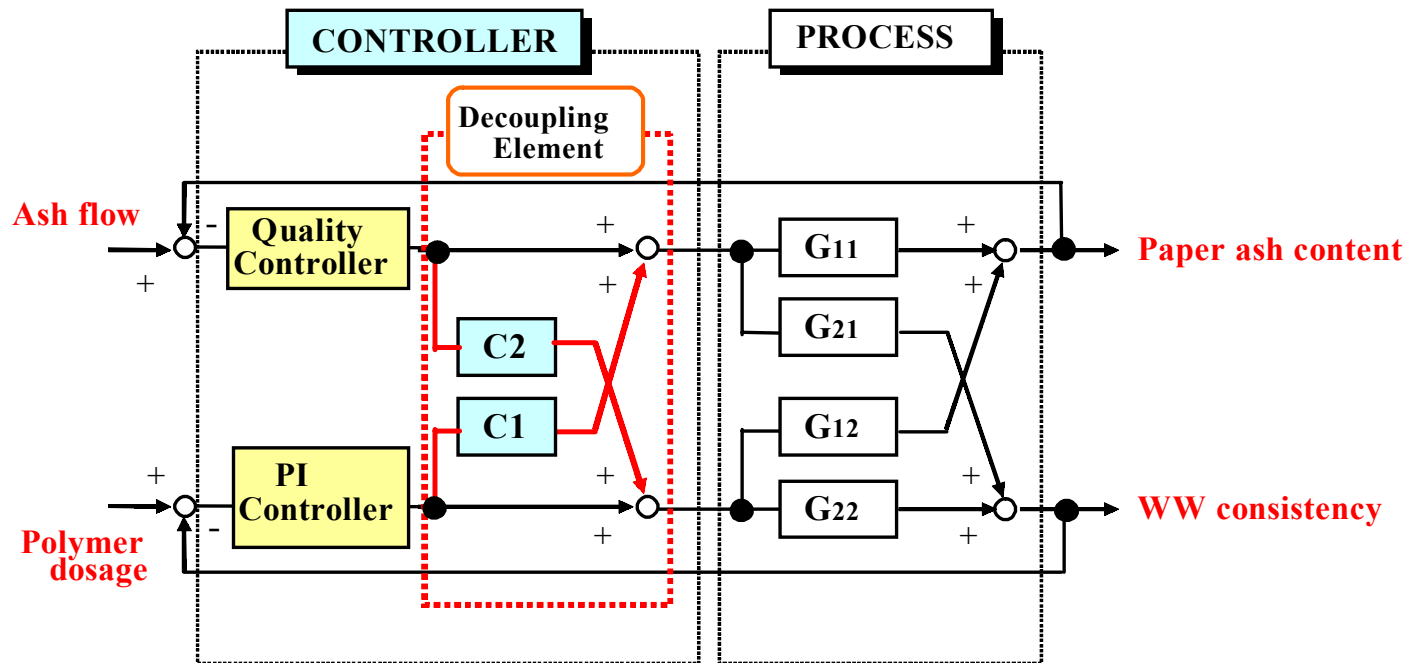
$$G_{21} = \frac{+ K_{21} \cdot e^{-90 \cdot S}}{1 + 780 \cdot S}$$

Polymer dosage

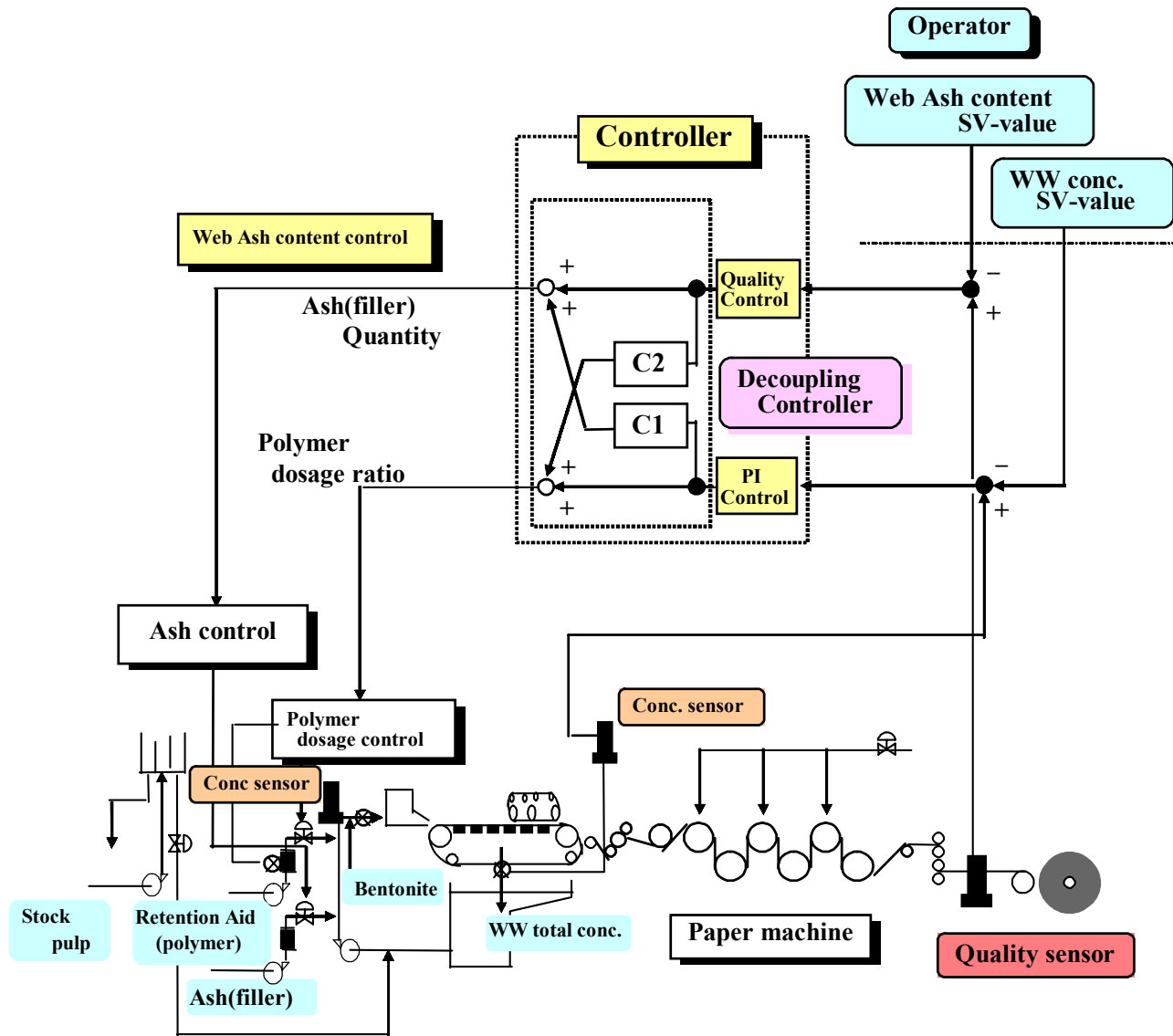
$$G_{12} = \frac{+ K_{12} \cdot e^{-174 \cdot S}}{1 + 828 \cdot S}$$

$$G_{22} = \frac{- K_{22} \cdot e^{-192 \cdot S}}{1 + 1164 \cdot S}$$

# Decoupling control



$$\left\{ \begin{array}{l} C1 = -\frac{G_{12}}{G_{11}} = -\frac{+K_{12} \cdot (I + 75 \cdot S)}{+K_{11} \cdot (I + 828 \cdot S)} \cdot e^{-48 \cdot S} \\ C2 = -\frac{G_{21}}{G_{22}} = -\frac{+K_{21} \cdot (I + 1164 \cdot S)}{-K_{22} \cdot (I + 780 \cdot S)} \cdot e^{+102 \cdot S} \end{array} \right.$$



**PI-control + Decoupling control**



## Decoupling control elements “C1” and “C2”

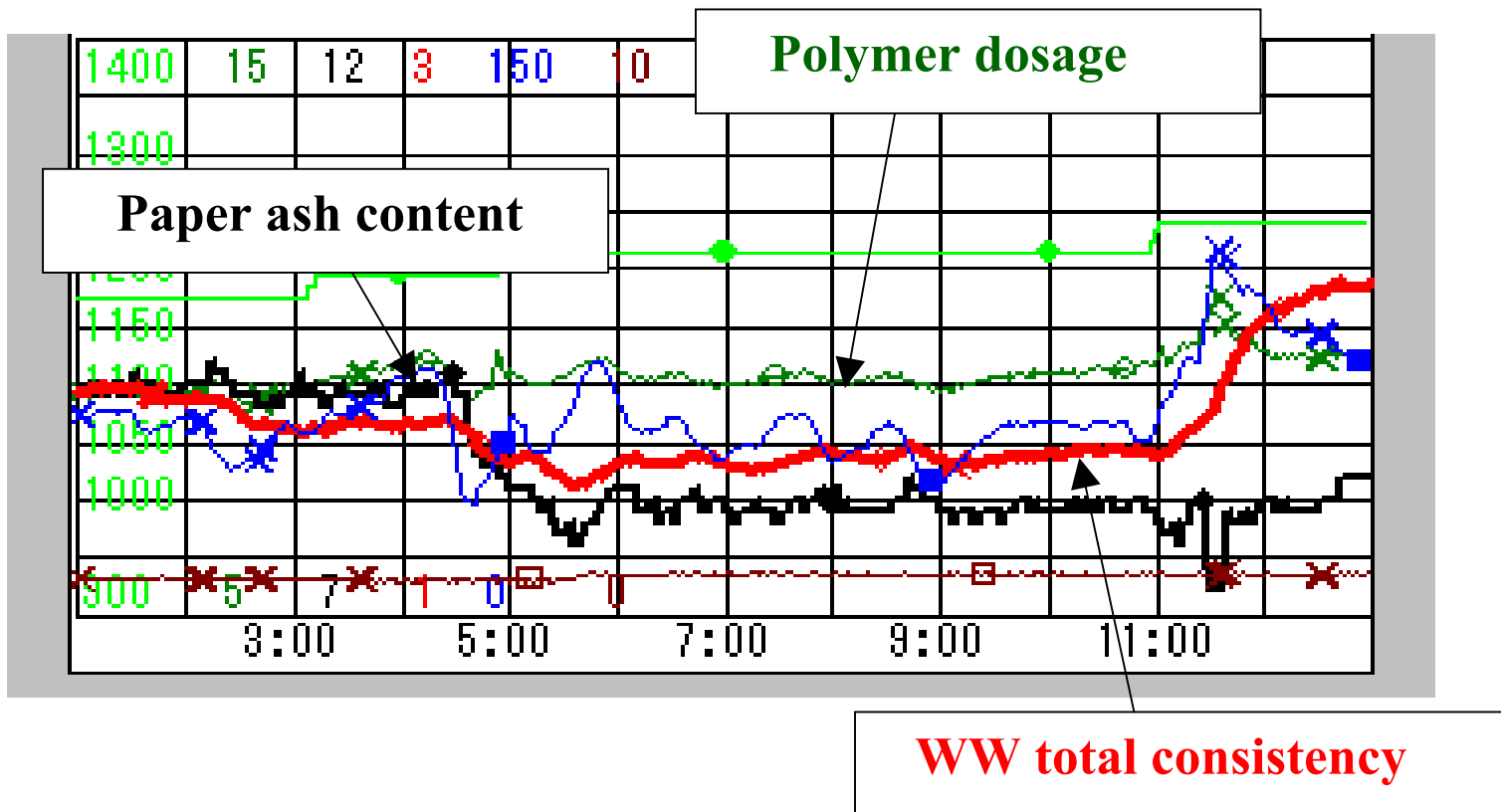
- Strategies to “**Robust**” and “**Simplify**” the Decoupling Controller .....

### “Steady-State Controller”.

$$C_2 = -\frac{+K_{21} \cdot (I + 1164 \cdot S)}{-K_{22} \cdot (I + 780 \cdot S)} \cdot e^{+102 \cdot S} \approx -\frac{+K_{21} \cdot (I + 1164 \cdot S)}{-K_{22} \cdot (I + 780 \cdot S)}$$
$$\approx -\frac{+K_{21}}{-K_{22}} = + \text{constant.}$$

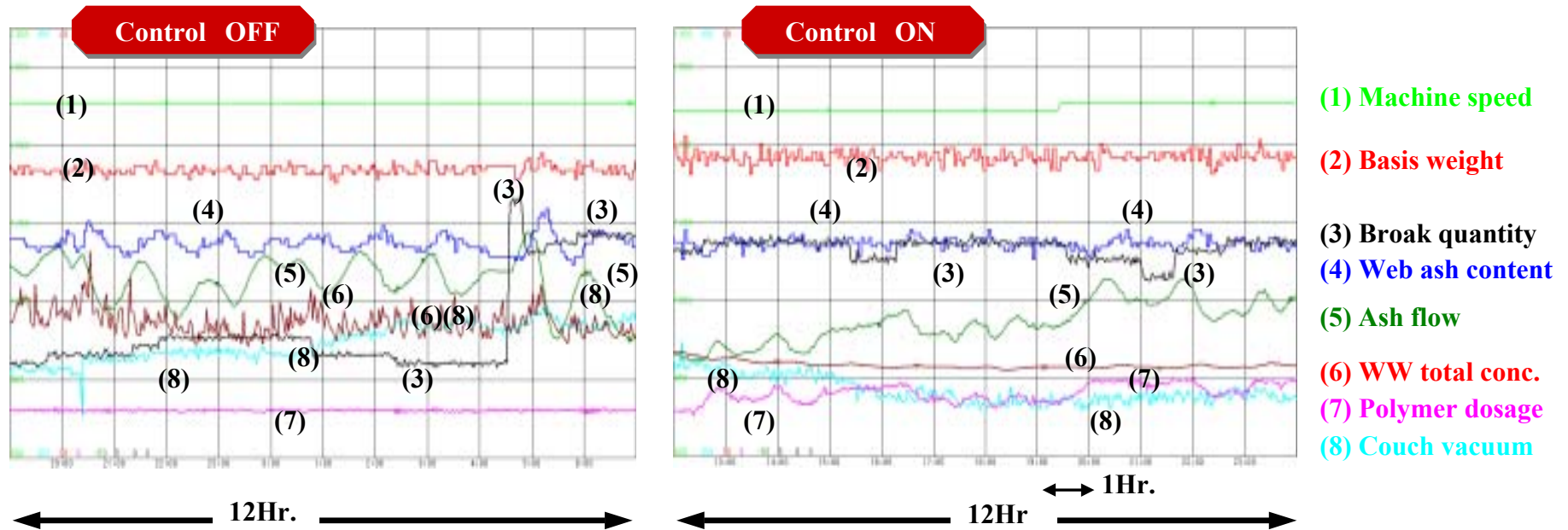
### “Partial Decoupling controller”.

$$C_1 = -\left( \frac{+K_{12}}{+K_{11}} \right) \cdot \frac{(I + 75 \cdot S)}{(I + 828 \cdot S)} \cdot e^{-48 \cdot S} \approx -0$$



**PI-control + Decoupling control**

## PI-control + Decoupling control result



- Stabilize the total consistency, ash flow of the wet-end section of a paper machine, and the ash content of the paper products.
- To alleviate the interaction problem, utilized a “decoupling controller” together with the “PI feed-back controller”.

## Summary

### ➤ control result ( *1sigma* : standard deviation )

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	<i>Before</i>	<i>After</i>	<i>Reduction (%)</i>
• WW consistency(%)	0.015	0.006	59 %
• Paper ash content (%)	0.13	0.10	21 %
• Ash flow (liter/min.)	9.49	7.56	20 %

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END

*Thank you for your attention.*

**[ ACKNOWLEDGEMENT ]**

We wishes to express their appreciation to Mr. S. Maki of *Metso Automation(Japan)* and, Mr. J. Nokelainen, Mr. T. Rantala, Mr. T. Huhtelin of *Metso Automation (Finland)* for their technical support and profitable discussions and advice.