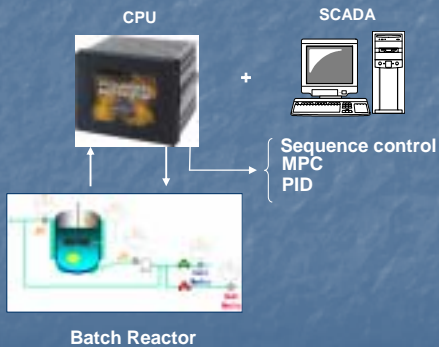


Model Predictive Control with Single Heat Transfer Fluid for Batch Reactor Temperature Control



Session MA2-17

[OS28]: Activities of SICE
Instrument and Control Engineers

JGC Corporation
Y.Noguchi

Are you really satisfied with
your controller Performance & its design environment?

Temperature controller performance:

- Most Dominant factor to determine **Product quality!!**
- We need a High performance Temp controller which runs on a **reliable platform** such as PLC.

However,

It is not easy to have a good controllability for:

- wide temperature range, e.g., - 50 to +150 Deg.C
- wide variety of products

It is not easy to design & Implement controller to PLC?

Are you really satisfied with your controller Performance & its design environment?

Why is it not easy to have a good controller?



- wide temperature range, e.g., - 50 to +150 Deg.C
- wide variety of products

Single Heat Media

This is because, Process Dynamics is changed by:

- Temperature range (No Control during Heat Media Change)
- Time
- Products

$$Time\ Const = \frac{\rho_m C_{p_m} V_m}{UA}$$

(Physical property & volume of the fluid inside the reactor change → Process Dynamics change.)

MPC

Why is it not easy to design & Implement controller?

- There is no user friendly controller design & implementation tool.

Reliable Controller

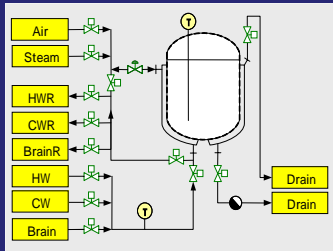
User Friendly Design Environment

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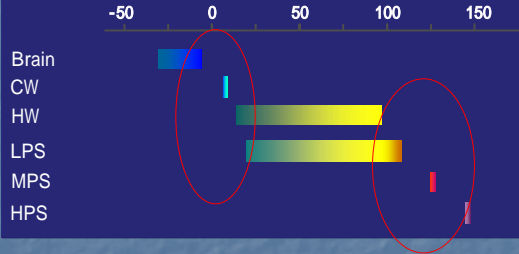
Multiple Heat Transfer Media
vs
Single Heat Transfer Media

Typical Batch Reactor Configuration

Multi Heat/Cool Media



Operation Range for Multiple Heat Media



Bad Temp. Controllability!

Why?: No temperature control during heating & cooling media change.

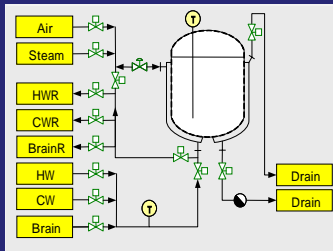
It is almost impossible to realize a good temperature controllability for batch reactor for wide temperature range during heating & cooling media change!!

Issues for Multiple Heat transfer Media

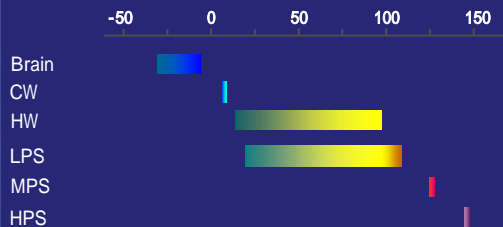
Other Issues:

1. Mix or loss of multiple heating and cooling media
2. Leak of multiple media to sewer (Environmental issue)
3. High probability of mis-operation caused by many valves

Multi Heat/Cool Media

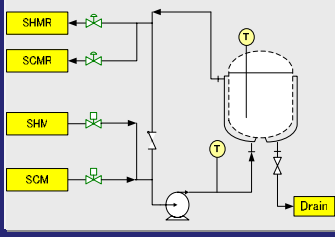


Operation Range for Multiple Heat Media



Single Heat Transfer Media System

Single Heat/Cool Media



Silicon Oil based
Heat Transfer Media

Other Advantages:

1. No Mix or loss of heating and cooling media
2. Less Leak of multiple media to sewer (Environmental Friendly)
3. Low probability of mis-operation by simple piping layout

Operation Range for Single Heat Media



Good Temp. Controllability!

Why?:

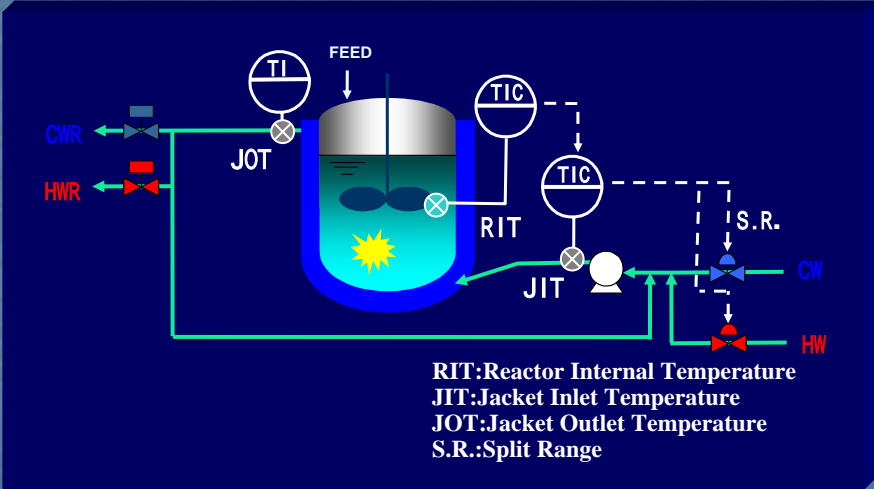
No heat transfer media change is required!

We can keep temperature controller mode in AUTO during batch operation continuously!

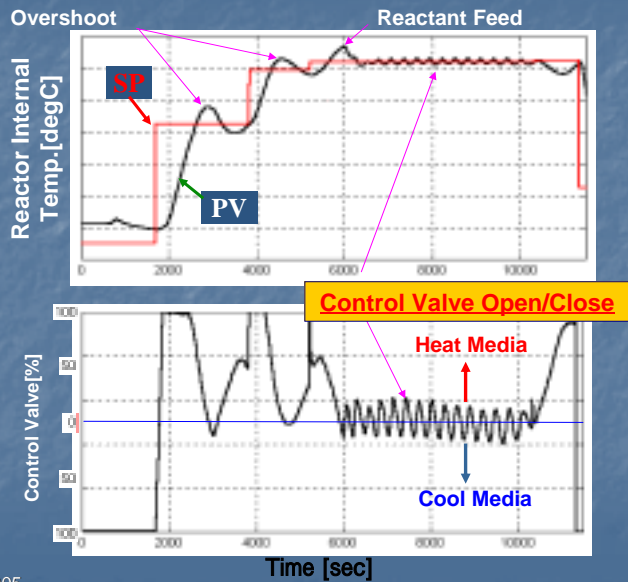
PID Controller
VS
Model Predictive Controller (PCR)

JGC's solution: **FlexThermo:**
MPC + Single Heat Transfer Media

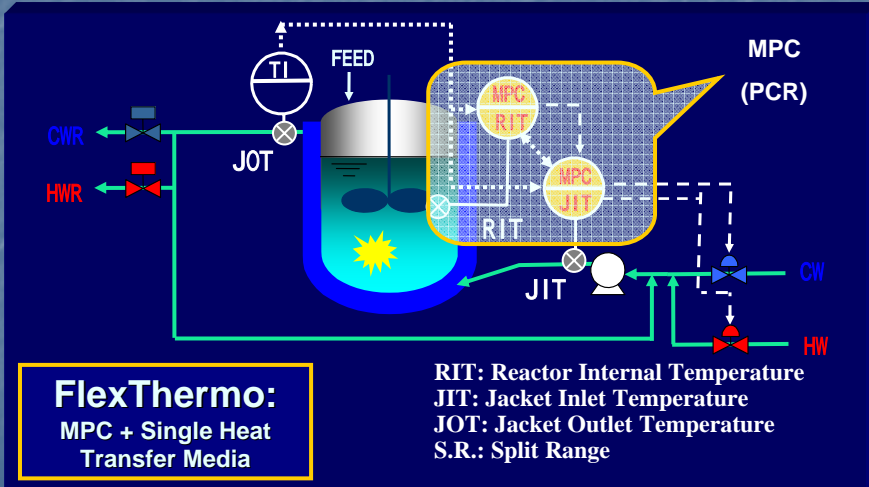
Typical Temperature Control Loop with PID controllers



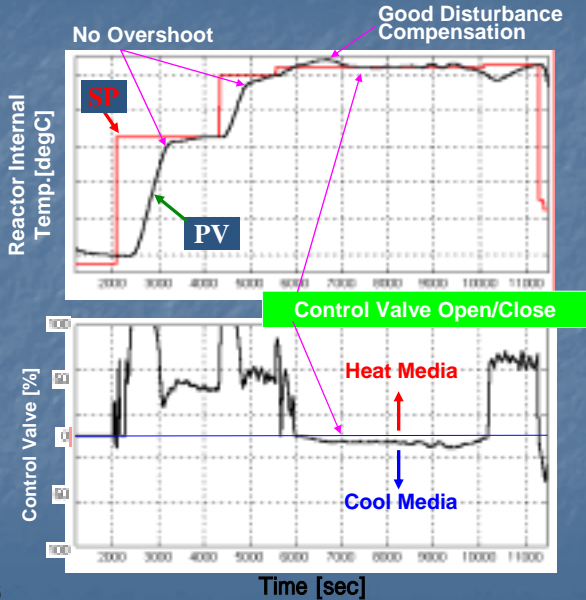
Trend Graph (PID)



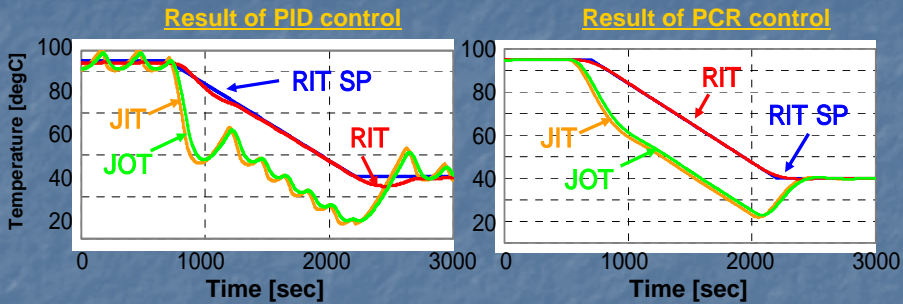
Typical Temperature Control Loop with MPC



Trend Graph (MPC)



Temperature Control for Crystallization (PID vs MPC)



Consumption ratio of hot and cold utility :

PID_hot / PCR_hot = 5.9 [-]
 PID_cold / PCR_cold = 8.1 [-]

Standard Deviation :

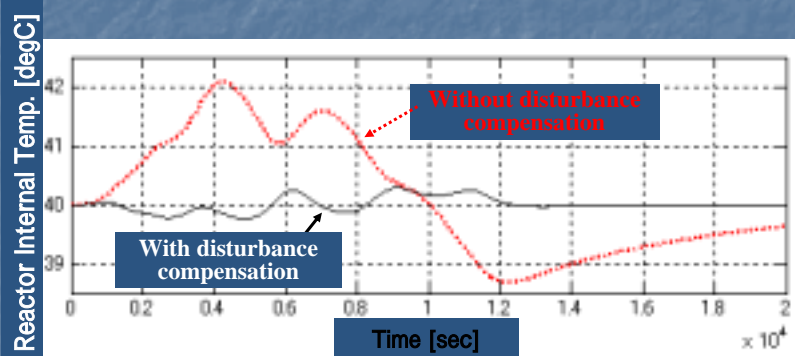
PID: 1.5 [degC]
 PCR: 0.4 [degC]

Maximum deviation from RIT SP :

PID: 4.9 [degC]
 PCR: 2.1 [degC]

83 – 88% Reduction of Utility Consumption with excellent controllability by MPC.

Result of the simulation with disturbance compensation



Why does MPC shows good controllability?

Why PID shows bad controllability?

This is caused by Process Dynamics change.

- Temperature range (No Control during Heat Media Change)
- Time
- Products

(Physical property & volume of the fluid inside the reactor change → Process Dynamics change.)

MPC (PCR introduced from Sherpa Engineering) shows good Controllability:

MPC Internal model parameter such as Time constant, Process gain can be updated based on:

- Temperature range (No Control during Heat Media Change)
- Time
- Products

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$$\text{MPC Internal Model Parameter Scheduling: } \text{Time Const} = \frac{\rho_m C_p V_m}{UA}$$

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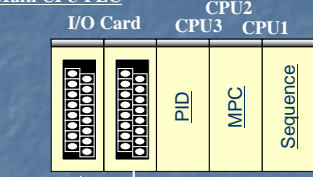
Multiple CPU Type Controller (PLC)
VS
Single CPU Type Controller



AD4820

Multiple CPU type Controller (PLC) Advantage & Disadvantage

Multi CPU PLC



Batch Reactor

Advantage of Multi-CPU PLC:

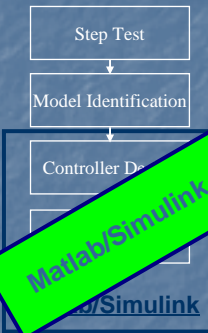
- Easy to expand the system capacity by adding required modules
- We can add required modules only.

Disadvantage of Multi-CPU PLC:

It takes time to implement the designed controller.

- Absolute Memory address handling
- Different data type between the CPUs
- Different design tools for each CPU
- Asynchronous signals between the CPU
- Not easy to configure integrated system, PID, MPC & Sequence controller
- Not easy to debug integrated system

Typical Implementation Steps to PLC

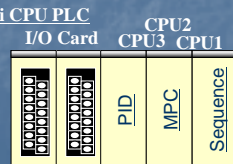
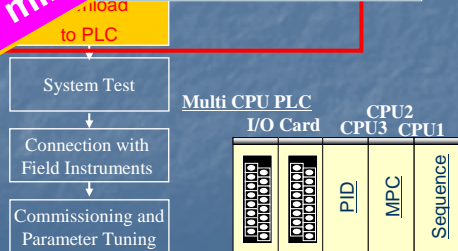


PLC Vendor's Controller Design

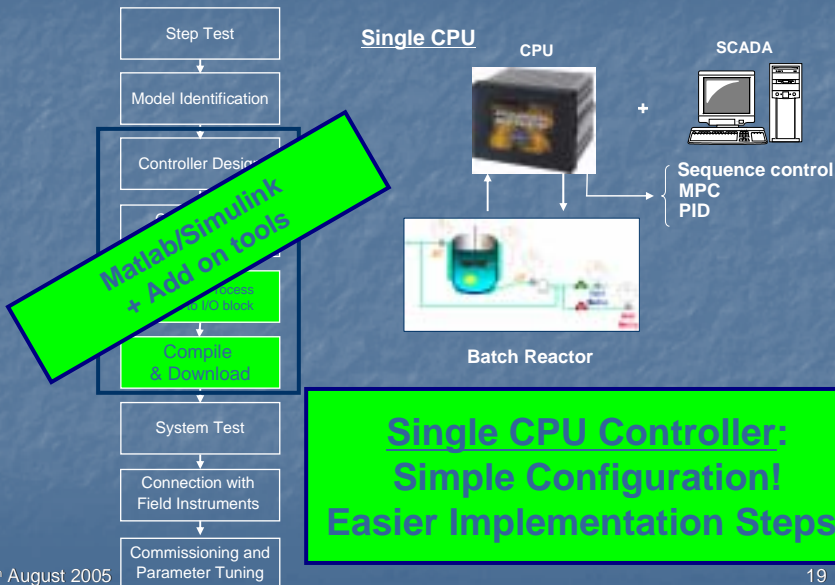
It takes time to implement the designed controller.

- Absolute Memory address handling
- Different data type between the CPUs
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- Asynchronous signals between the CPU
- Not easy to configure integrated system, PID, MPC & Sequence controller
- Not easy to debug integrated system

Time consuming process!!
Can we minimize this process?

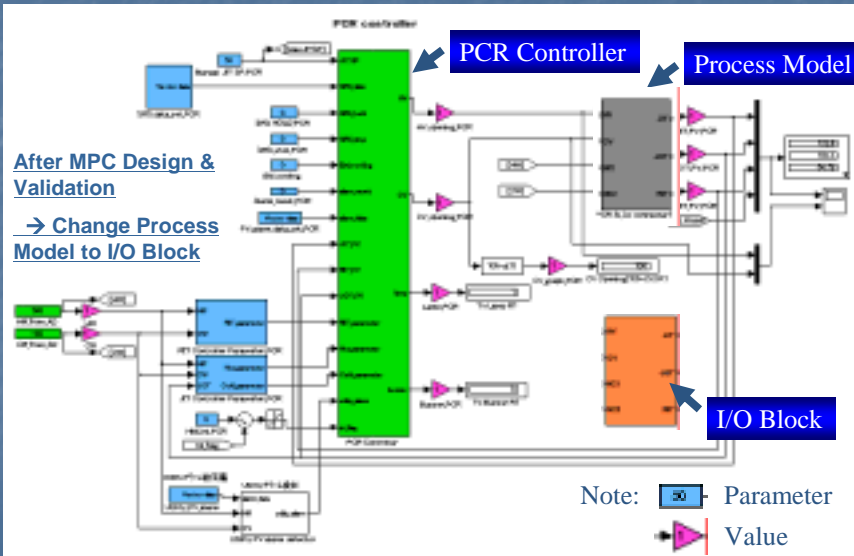


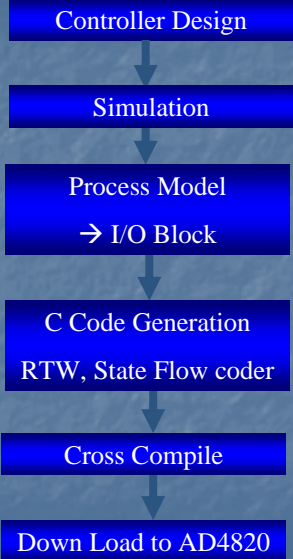
Implementation Steps to Single CPU Controller



**Single CPU Controller:
Simple Configuration!
Easier Implementation Steps!**

MPC Design by Matlab/Simulink





Simulink + Add on

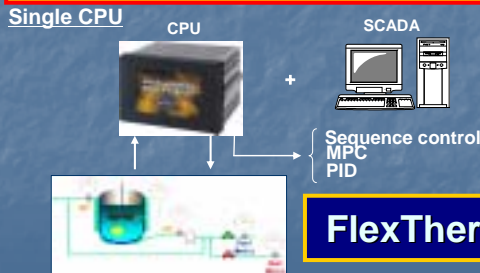
Control engineer can concentrate on controller design by using Matlab/Simulink design environment not only design and simulation but also for controller implementation on target computer, i.e., AD4820!

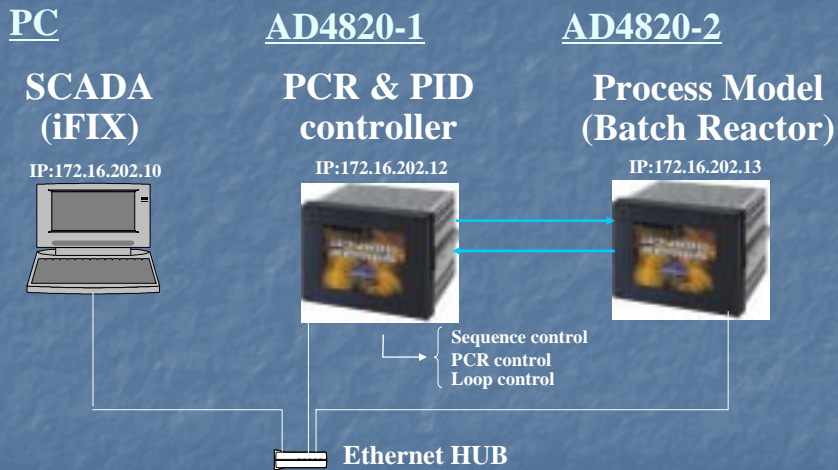
Solution:

Combination of:

1. Silicone Oil Based Single Heat Transfer Media
2. MPC (PCR introduced from Sherpa Engineering)
3. Reliable A&D's Controller (ADX) with User friendly Simulink based Design Environment

Designer can concentrate on Controller design!





Any Questions?

Yoshikazu Noguchi
Information Technology Department
JGC Corporation
URL: www.jgc.co.jp
Email: noguchi.yoshikazu@jgc.co.jp

PCR ?

バッチリアクター温度制御向けに開発されたモデル予測制御パッケージ

- 開発元/販売元: Sherpa Engineering (France)
- 制御対象: バッチ反応器、熱交換器の温度制御
- プラットフォーム: PLC・DCS・PC・プロコン等
- 制御アルゴリズム: モデル予測制御
- モデル: 一次遅れ+無駄時間モデル

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PCRの特徴(1)内部モデル

- 内部モデル: 1次遅れ + 無駄時間モデル

$$Gp(s) = K \frac{e^{-Ds}}{1 + Ts}$$

K: ゲイン[-]
 T: 時定数[sec]
 D: 無駄時間[sec]

- 制御アルゴリズムに収束計算がなく、C言語で記述
 - ➔ PLC, PC, DCS, プロコンで動作可能
- 物理的なパラメータと内部モデルとの関連付けが容易
 - ➔ レシピに応じた内部モデルのパラメータ設定

$$T = \frac{\rho_m C_{p_m} V_m}{UA}$$

m: 密度[kg/m³]
 C_{pm}: 定圧比熱 [J/kg/]
 V_m: 反応器内容積[m³]
 U: 総括熱伝達係数[J/sec/m²/]
 A: 伝熱面積[m²]

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